

OLIGO-GLUCOMANNAN PRODUCTION FROM PORANG (*Amorphophallus oncophyllus*) GLUCOMANNAN BY ENZYMATIC HYDROLYSIS USING β -MANNANASE

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ABSTRACT: Porang (*Amorphophallus oncophyllus*) is an indigenous tuber of Indonesia that rich in glucomannan. An alternative approach to produce porang oligo-glucomannan (POG) as prebiotic from porang glucomannan (PGM) was made by enzymatic hydrolysis using β -mannanase. This study aimed to produce POG under optimal conditions by controlled enzymatic hydrolysis process. The PGM flour contained 96.12% of indigestible carbohydrates. The optimum condition of enzymatic hydrolysis producing the highest reducing sugar was as follows: temperature 37 °C, pH 5.5, a ratio of enzyme to the substrate (E/S) 1:1000, and reaction time 4 h. HPLC analysis confirmed that 99.45% of the resulting POG consisted of oligosaccharides with a degree of polymerization (DP) 3. Hence, the PGM utilized in this study has been proven as a potential substrate for POG production. Additionally, the resulting POG was considered as a functional ingredient due to has prebiotic potential.

Keywords: Porang glucomannan, oligo-glucomannan, prebiotic, β -mannanase, functional ingredient.

INTRODUCTION

Porang is a parental plant in Indonesia which belongs to the genus *Amorphophallus* of the *Araceae* family. Its bulb has glucomannan rich up to 75.72% in porang flour (Safitri *et al.*, 2014) and 90.98% in porang tuber (Yanuriati *et al.*, 2017). Although, the high yield of glucomannan is obtained by extraction from dried porang tuber but for industrial scale production prefers extraction from fresh porang tuber due to no drying process is needed thus lower cost of production (Yanuriati *et al.*, 2017).

Glucomannan is a polysaccharide consist of β -1,4 linked D-glucose and D-mannose residue with short branches of β -1,6-glycosyl units which is attached at the C-3 position of a sugar unit (Lin *et al.*, 2010). The konjac glucomannan (KGM) has been useful in the biological functions such as constipation mitigation, control of blood glucose and cholesterol level, antioxidant, anti-inflammatory, bio-adhesive supplements, and medical implants (Behera and Ray, 2016).

However, the glucomannan application is still limit in expand the functionality in order to its high viscosity and molecular weight, those are responsible for low bioavailability (Ojima *et al.*, 2009). Unfavorable characteristics of it for the food field and pharmaceutical industries (Zhang *et al.*, 2005; Hu *et al.*, 2009). Hence, the porang glucomannan needs to be processed prior to the applications by hydrolyzing the polysaccharides into oligosaccharides. The hydrolysis can be performed by a selected method considering reaction conditions, safety and cost (Yan *et al.*, 2018; de Moura *et al.*, 2014). So, PGM needs processing further with hydrolysis process It is selected based on the performance and considering

of reaction conditions, safety and cost (de Moura *et al.*, 201; Yan *et al.*, 2018).

The oligosaccharide production allows to expose on large scale using enzymatic hydrolysis. In the literature, enzymatic process is the best option for oligosaccharides production due to its reproducibility (de Moura *et al.*, 2014). According to Du *et al.* (2011) oligosaccharides are mostly produced by either the enzymatic hydrolysis or transglycosylation. These method have been applied based on contribution attributes such as a low energy and safe process (Liu *et al.*, 2015). Hence, this study aimed to develop oligo-glucomannan production and its quality through PGM hydrolysis using β -mannanase.

MATERIALS AND METHODS

Materials

Porang glucomannan (PGM) flour was supplied by the Faculty of Agricultural Technology, Universitas Gadjah Mada, Yogyakarta, Indonesia. β -mannanase was purchased from Mianyang Habio Bioengineering Co., Ltd., Sichuan, China. Sodium acetate was obtained from Sigma-Aldrich Co., St. Louis, USA. Sodium hydroxide was obtained from Loba Chemie, Pvt, Ltd., Mumbai, India.

Methods

Optimization of porang oligo-glucomannan (POG) production

PGM flour (1% w/v) was added into 0.2 M CH₃COONa (sodium acetate buffer) and then mixed with β -mannanase. The concentrations of the enzyme to substrate ratio (E/S) were 1:4000, 1:2000, 1:1000 (w/w). The mixture was stirred continuously in an air incubator shaker at various

pH (5.2, 5.5, and 5.8). The temperature was set at 28, 37 or 48 °C by the air incubator shaker. In PGM incubation was monitored for 12 h and samples were taken at 2, 4, 6, and 12 h. The last step, samples were boiled for 10 min to inactivate the enzyme then centrifuged at 8,000 g to remove the enzyme.

Proximate analysis

The effectiveness PGM as main material was analyzed to measure the physicochemical properties such as moisture, protein, lipid, crude fiber, and ash contents according to the recommended method by AOAC (1995).

Sugar analysis

Analysis of total sugar was performed according to the phenol-sulphuric acid method proposed by Dubois *et al.* (1956) with some modifications for the sample preparation. The sample was diluted 10 to 20 times and a solution of 5% phenol reagent was added. The reducing sugar was analyzed by the DNS method (Miller, 1959). One unit of mannanase was an enzyme that released one µg of mannose equivalent per minute (Dubois *et al.*, 1956; Miller, 1959).

The degree of polymerization analysis

Analysis of total sugar was conducted based on the phenol-sulphuric acid method. The degree of polymerization (DP) was determined by the ratio of total sugars and reducing sugars.

$$DP = \text{Total Sugar} / \text{Reducing Sugar}$$

Oligosaccharides analysis

The sample was diluted to reach concentration within the available calibration curve of the standard reference. Prior to the injection into high-performance size exclusion chromatography (HPSEC; Agilent model 1200 series, CA, USA), the sample was filtered through a 0.22 µm syringe filter. The injection volume was 20 µl. The flow rate of the mobile phase (distilled water) was set at 1 ml min⁻¹. The setting temperature for the RI detector was 30 °C. The acquired data was recorded by Chem Station software (Agilent Technologies) to estimate the concentration of POG that comprised of polymer, oligomer, and monomer fractionations.

Statistical Analysis

The effect of the studied variables on the PGM hydrolysis was determined by a one-way analysis of variance (ANOVA). The statistical significance level was set to $p < 0.05$ for the significances. In the event that the effects were significant, post hoc test was calculated. The data were presented as mean ± standard deviation (SD).

RESULTS AND DISCUSSIONS

Proximate analysis

The proximate analysis of porang glucomannan is reported in Table 1. The result was founded in PGM contained high carbohydrate (96.12%) which mainly polysaccharide as claimed glucomannan. It was calculated based on the dry weight of the PGM. According to Harmayani *et al.* (2014), PGM flour contains glucomannan almost the same around

92.69% of glucomannan. Meanwhile, the glucomannan content in porang powder roughly of 75.72% (Safitri *et al.*, 2014). As a result that PGM was consisted of lipid (2.52 g/100 g ±0.10), crude fiber (0.37 g/100 g ±0.05), protein (0.33 g/100 g ±0.08), ash (0.66 g/100 g ±0.02) and water (8.48 g/100 g ±0.15). As a comparison, the purity of glucomannan of the extracted porang tuber is enhanced to 90.98% with a low percentage of ash (0.57%) and protein (0.61%) without starch content (Yanuriati *et al.*, 2017).

Table 1. The chemical composition of porang glucomannan (PGM) flour.

Composition	Content (g/100g, db)
Water	8.48±0.15
Ash	0.66±0.02
Lipid	2.52±0.10
Protein	0.33±0.08
Crude fiber	0.37±0.05
Carbohydrate	96.12±0.05

Values are means ± SD from duplicate analysis

Effect of temperatures on POG production

The results of the enzymatic hydrolysis of porang glucomannan powder on the different times are shown in Table 2. The temperatures were varied set at 28 °C, 37 °C, and 48 °C, while other parameters were fixed at pH 5.5, time of 12 h, and ratio enzyme to substrate 1:2000 (w/v). The result showed oligosaccharides were not obtained within 2 h incubation at 28 °C but increasing gradually incubation time during 6-12 h. It was contrary to the trend at 37 °C and 48 °C. However, the depolymerization of PGM at 37 °C took time very quickly after 2 h and elevating gradually during incubation time while no producing the oligosaccharide at 48 °C was observed after 2 h. The oligosaccharides (%) at 37 °C showed significantly increased ($p < 0.05$) after 2 h and kept maintained during 12 h. Oligosaccharides were produced under the prediction of optimum temperature in a short period incubation time compared to one of the treatments described above (48 °C). It was according to Ariestanti, *et al.* (2018) reported the highest concentration of oligosaccharide production with lower molecular weight was at the condition of 48 °C

Considering the optimum temperature in enzymatic hydrolysis might not allow too high, because it has been affecting on the denaturation of the enzyme. According the literature that the decreased hydrolytic efficiency of β-mannanase was probably inactivated with increasing time. Consequently, the temperature and time in this study was chosen based on present oligosaccharide in the beginning time with gaining a yield. Moreover, the optimum temperature was chosen at 37 °C. However, another study demonstrated that there are some aspects on influencing β-mannanase activity such as substrate concentration, the yield product, and inactivating enzyme (Liu *et al.*, 2015). They also reported that oligosaccharides could be produced by enzymatic hydrolysis at room temperature reflected in this study that produced oligosaccharides at 28 °C but took a long time of incubation.

Table 2. The oligosaccharides content (%) at various temperature of POG production analyzed by high performance size exclusion chromatography (HPSEC).

Temperature	Yield (%)			
	Poly-	Higher oligo-	Oligo-	Mono-
28 °C				
2	72.82 ± 0.16 ^a	ND	ND	27.19 ± 0.16 ^a
4	0.27 ± 0.01 ^b	74.45 ± 0.08	ND	25.29 ± 0.07 ^b
6	0.36 ± 0.01 ^b	ND	75.04 ± 0.07 ^b	24.60 ± 0.07 ^c
12	0.21 ± 0.08 ^b	ND	76.24 ± 0.15 ^a	23.56 ± 0.15 ^d
37 °C				
2	0.20 ± 0.12 ^b	ND	69.82 ± 3.99 ^{ab}	29.99 ± 3.87 ^{ab}
4	0.47 ± 0.12 ^a	ND	74.64 ± 0.90 ^a	24.40 ± 0.07 ^{ab}
6	0.27 ± 0.02 ^{ab}	ND	72.60 ± 1.89 ^{ab}	27.14 ± 1.87 ^b
12	0.41 ± 0.01 ^{ab}	ND	66.27 ± 1.33 ^b	33.32 ± 1.32 ^a
48 °C				
2	1.63 ± 1.72 ^a	72.94 ± 0.68	ND	25.44 ± 1.04 ^b
4	0.08 ± 0.05 ^a	ND	67.34 ± 0.48 ^b	32.59 ± 0.43 ^a
6	0.17 ± 0.16 ^a	ND	72.20 ± 2.29 ^a	27.64 ± 2.45 ^b
12	0.28 ± 0.01 ^a	ND	74.17 ± 0.21 ^a	25.56 ± 0.21 ^b

Values are means ± SD from duplicate incubation in % area, ND = not detected
 Different letters following mean values within the same column indicate significant differences at the p<0.05.

Effect of pH on POG production

The results of the enzymatic hydrolysis of porang glucomannan on the different pHs were shown in Table 3. The hydrolysis process was carried out at a pH of 5.2, 5.5, and 5.8, while other reaction conditions were set as optimum temperature chosen at 37 °C, enzymatic concentration 1:2000 (w/v) for 12 h. In each condition was found oligosaccharide, but whether the pH was set at 5.5, showing the oligosaccharide in a short incubation time (2 h). Meanwhile, the opposite trends were observed at 5.2 and 5.8. They showed oligosaccharide production was found after 4 h and not presence in the beginning of incubation time. Thus, the optimum pH for the hydrolysis

of PGM was 5.5. It was represented the oligosaccharides obtain in a short period and increased significantly (p<0.05) after 2 h. Usually, the activity and stability of β-mannanase from various bacteria are optimum in acidic pH range (5-6). In the term of PGM hydrolysis, the optimum pH was at 5.5. In hydrolysis, the activity and stability of enzymes are different depending on typical of buffer composition for maintaining pH in the reaction (Liu *et al.*, 2015). As a result, a pH of 5.5 of acetate buffer was a value reasonably well with literature previously demonstrated by Ariestanti *et al.* (2018) and favored with the company requirement of enzyme used.

Table 3. The oligosaccharides content (%) at various pHs of POG production analyzed by high performance size exclusion chromatography (HPSEC).

pH	Yield (%)			
	Poly-	Higher oligo-	Oligo-	Mono-
5.2				
2	0.29 ± 0.25 ^a	76.57 ± 2.79	ND	23.15 ± 2.55 ^b
4	0.51 ± 0.01 ^a	ND	74.61 ± 1.29 ^a	24.89 ± 1.28 ^{ab}
6	0.35 ± 0.22 ^a	ND	73.94 ± 2.76 ^a	25.72 ± 2.54 ^{ab}
12	0.30 ± 0.16 ^a	ND	70.12 ± 0.40 ^a	29.59 ± 0.56 ^a
5.5				
2	0.20 ± 0.12 ^b	ND	69.82 ± 3.99 ^{ab}	29.99 ± 3.87 ^{ab}
4	0.47 ± 0.12 ^a	ND	74.64 ± 0.90 ^a	24.40 ± 0.07 ^{ab}
6	0.27 ± 0.02 ^{ab}	ND	72.60 ± 1.89 ^{ab}	27.14 ± 1.87 ^b
12	0.41 ± 0.01 ^{ab}	ND	66.27 ± 1.33 ^b	33.32 ± 1.32 ^a
5.8				
2	0.26 ± 0.05 ^{ab}	79.15 ± 0.12	ND	20.60 ± 0.07 ^a
4	0.13 ± 0.01 ^c	ND	84.92 ± 5.90 ^a	14.96 ± 5.91 ^a
6	0.15 ± 0.01 ^{bc}	ND	81.70 ± 0.89 ^a	18.15 ± 0.91 ^a
12	0.26 ± 0.06 ^a	ND	82.16 ± 2.57 ^a	17.59 ± 2.62 ^a

Values are means ± SD from duplicate incubation in % area, ND = not detected
 Different letters following mean values within the same column indicate significant differences at the p<0.05.

Effect of the enzyme to substrate (E/S) ratios on POG production

The results of the enzymatic hydrolysis of porang glucomannan with the different enzyme concentrations are shown in Table 4. Enzyme concentrations were set at 1:4000, 1:2000, and 1:1000 (w/v), while other hydrolysis variables were set as the temperature of 37 °C, pH of 5.5 for 12 h of incubation time. Escalating ratio enzyme to substrate tends to expand in oligosaccharide production (Chen *et al.*, 2013). When E/S was at 1:1000 (w/v), the oligosaccharide was attained after 2 h and a highly significant ($p < 0.05$) after 4 h with a low monosaccharide concentration (0.46%), but no further significant increasing. Hence, the optimum ratio enzyme per substrate is 1:1000 (w/v) for 4 h of incubation. The result showed an additional E/S ratio acquiring oligosaccharide production in order to attach

substrate properly to gain product. Although, the ability of the enzyme could be decreased by diminishing viscosity of substrate concentration addition (Liu, *et al.* 2015). They suggested that the glucomannan hydrolysis has to prove the amount of glucomannan with enzyme ratio. It relates to the ability of endo β -mannanase cleaved the β -1,4 linkages on the whole substrate (Alonso-Sande *et al.*, 2009; Al-Ghazzawi *et al.*, 2012; Jian *et al.*, 2013). In this study resulted in the minor of polysaccharide and monosaccharide as an undesirable compound is not necessary purification processes for eliminating them. Moreover, the result was claimed its optimum ratio enzyme to substrate produced the oligosaccharides as dominant compound comparing with others, consequently the purification should be not an option in POG production.

Table 3. The oligosaccharides content (%) at various pHs of POG production analyzed by high performance size exclusion chromatography (HPSEC).

E/S ratio	Yield (%)			
	Poly-	Higher oligo-	Oligo-	Mono-
1:4000				
2	0.43 ± 0.01 ^a	69.81 ± 2.88 ^a	29.20 ± 2.96 ^b	0.57 ± 0.08 ^c
4	0.28 ± 0.04 ^b	79.79 ± 6.91 ^a	19.16 ± 6.49 ^b	0.78 ± 0.38 ^c
6	0.31 ± 0.03 ^b	ND	90.58 ± 1.10 ^a	9.12 ± 1.07 ^b
12	0.20 ± 0.01 ^c	ND	81.95 ± 0.49 ^a	17.85 ± 0.49 ^a
1:2000				
2	0.20 ± 0.12 ^b	ND	69.82 ± 3.99 ^{ab}	29.99 ± 3.87 ^{ab}
4	0.47 ± 0.12 ^a	ND	74.64 ± 0.90 ^a	24.40 ± 0.07 ^{ab}
6	0.27 ± 0.02 ^{ab}	ND	72.60 ± 1.89 ^{ab}	27.14 ± 1.87 ^b
12	0.41 ± 0.01 ^{ab}	ND	66.27 ± 1.33 ^b	33.32 ± 1.32 ^a
1:1000				
2	0.20 ± 0.05 ^a	99.35 ± 0.02	ND	0.46 ± 0.03 ^a
4	0.17 ± 0.05 ^a	ND	99.45 ± 0.09 ^{ab}	0.39 ± 0.04 ^a
6	0.24 ± 0.11 ^a	ND	99.38 ± 0.04 ^b	0.39 ± 0.08 ^a
12	0.16 ± 0.03 ^a	ND	99.75 ± 0.13 ^a	0.10 ± 0.12 ^b

Values are means ± SD from duplicate incubation in % area, ND = not detected. Different letters following mean values within the same column indicate significant differences at the $p < 0.05$.

Degree polymerization of POG

In the optimum condition was found the value of total sugar was 9.85 mg/ml, and the amount of reducing sugar was 2.93 mg/ml, so the amount of DP was 3. The reducing sugar of POG was obtained under optimal conditions (1:1000 of E/S, 5.5 pH, and 37 °C) is summarized in Figure 1. The amount of reducing sugar shows the ability of mannanase to hydrolyze porang glucomannan (Safitri *et al.*, 2014). Accordingly, Chen *et al.* (2013) reported that oligosaccharides production is influenced precisely by reducing sugar present.

More recent studies reported that DP of oligosaccharides produced by all kinds of substrates using enzyme mannanase indicated enzyme capability is restrict to only degrading substrate into oligosaccharide such as mannobiose and not further activity to get small compound (Safitri *et al.*, 2014). Notably, Jian *et al.* (2013) successfully applied the prolonged incubation time in hydrolysis could obtain oligosaccharide of DP 4-5 into DP 2-3. It was the same in

porang glucomannan hydrolysis which produced the same degree of polymerization in range of 3-4. According to Zhang *et al.* (2009) that konjac flour hydrolyzed by mannanase of *Bacillus* spp. MSJ-5 produces manno-oligosaccharides with DP 2-6 and Liu *et al.* (2015) found that KOG prepared by degrading konjac glucomannan using β -mannanase is 5.2 of DP, with the small molecule and high antioxidant activity..

So, in the present study indicated that PGM was successfully hydrolyzed by using β -mannanase produced DP of POG with lower chain length than its native which prepared by cabinet drying (DP 9.4) and by freeze-drying (DP 12) (Harmayani *et al.*, 2014).

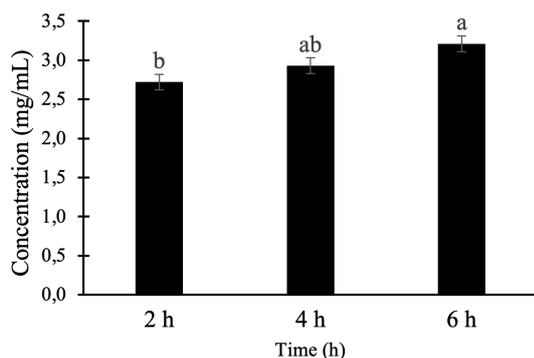


Figure 1. The reducing sugar concentration under optimal conditions (1:1000 or 0.1% E/S, 5.5 pH, and 37 °C).

CONCLUSION

Porang oligo-glucomannan (POG) was successfully produced by controlled hydrolysis conditions of porang glucomannan (PGM) under optimal conditions. The optimal conditions were 37 °C, pH 5.5, E/S of 1:1000 or 0.1% (w/v) and reaction time for 4 h. The POG was yielded of 94.45% with minor contents of polysaccharides and monosaccharides mixture. The majority of POG had DP in the range of 3-4. The results of this study suggested of POG to be applied as prebiotic ingredients in the food industry, due to it is practical for industrial-scale production with high productivity and low cost of production without a purification step. We believe that knowledge gained from this study will help to exploit further and improve the utilization value of porang glucomannan and provide theoretical support for the development of health food in the human study further.

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